

# CO<sub>2</sub> utilisation

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# Overview

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- > Differences with storage
- > Physics: miscibility, dispersion, temperature
- > Enhanced Oil Recovery
- > Enhanced Gas Recovery
- > Concluding remarks

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# What are those physical phenomena?



## Transport phenomena

- > Viscous forces
- > Diffusive forces
- > Gravity forces
- > Capillary forces
- > Mobility control

## CO<sub>2</sub> specific aspects

- > Three non-aqueous phases
- > Chemical interaction with reservoir rock
- > Supercritical behaviour

## Compositional aspects

- > Swelling of oil
- > Condensing / vaporising gas drive
- > Miscibility development - IFT effects
- > Miscibility in water

## Rock properties

- > Reservoir compaction/dilation
- > Sealing faults
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## Compositional aspects:

- > CO<sub>2</sub> may evaporate hydrocarbons into mobile CO<sub>2</sub>-rich phase;
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## Miscibility in water:

- > CO<sub>2</sub> is soluble in water - much higher solubility than for methane or nitrogen (additional safe storage);
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!!! CO<sub>2</sub> injection significantly increase precipitation of heavy hydrocarbons like asphaltines - this **must** be investigated.

# Evaluation of CO<sub>2</sub> injection



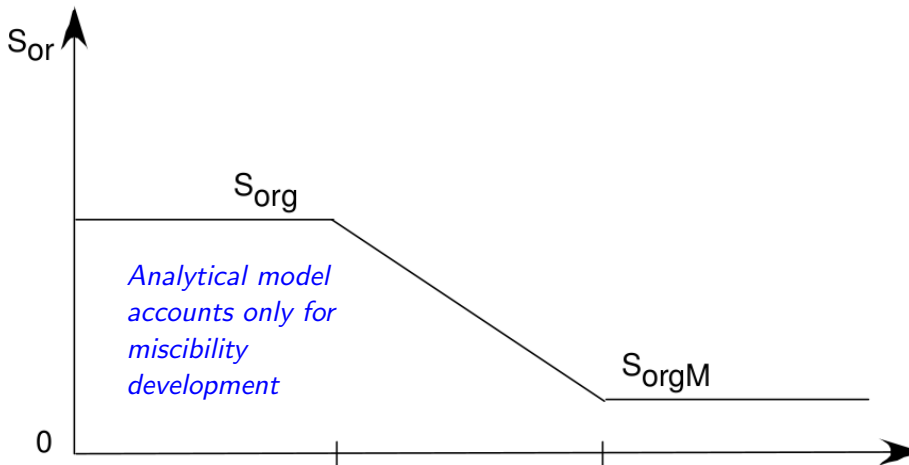
To evaluate applicability of the CO<sub>2</sub> to particular field an analytical package like SWORD could be used

*Analytical model  
accounts only for  
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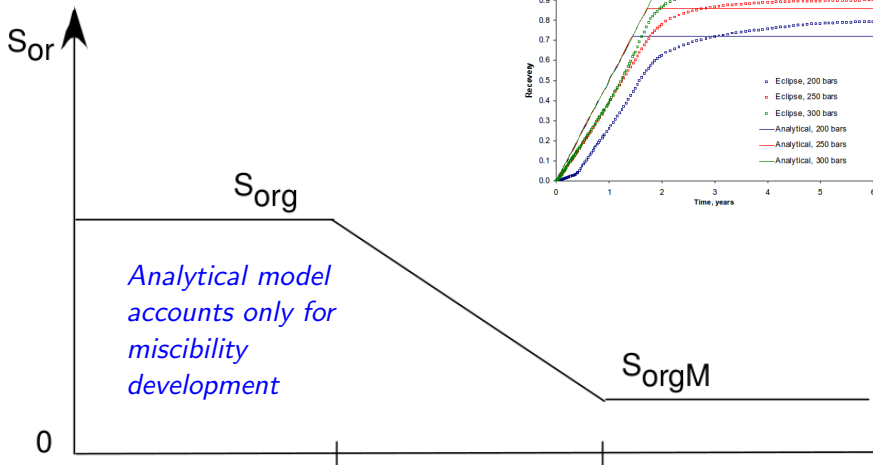




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# EOR: analytic screening. Expert system



Welcome, Ext user!

Load Save Reports Profile Help Logout

## Applicability screening

- Field case input
- Applicability evaluation
- Reference intervals

## Recovery factor estimation

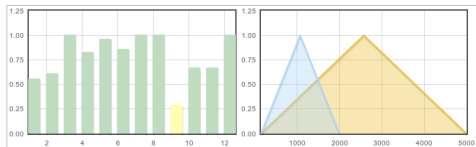
## Performance prediction

## Thermal recovery

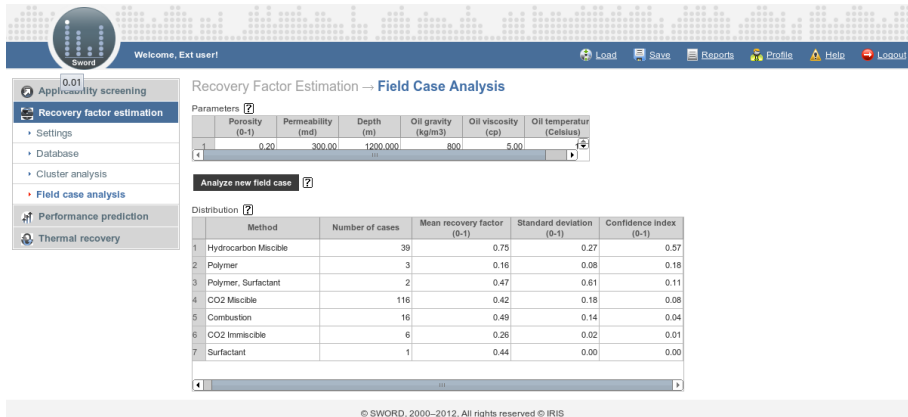
## Applicability screening → Applicability evaluation

Method	Score	Violations
Gas injection	0.784	0
Chemical methods	0.735	0
Water flooding	0.576	0
Thermal methods	0.576	0

Parameter	Unit	User			Reference intervals			Score
		Min	Max	Comfort center	Min	Max	Comfort center	
Depth	m	150	2000	1075	150	5000	2575	0.552
Permeability	md	100	2000	1050	1	5000	2500.5	0.606
Thickness	m	6	20	13	2	130	10	0.999
Temperature	Celsius	0	70	35	0	100	50	0.824
Oil viscosity	cp	1	10	5.5	0.2	10	5.1	0.957
Pressure	bar	140	290	215	80	500	290	0.854
Oil density	kg/m3	750	850	800	650	950	800	1
Anisotropy (kv/kh)	(0-1)	0.01	0.1	0.055	0.01	0.1	0.055	1
Clay content	(0-1)	0	0.05	0.025	0	0.3	0.15	0.286
Salinity	kg/m3	0	20	10	0	40	20	0.667
Curr/init oil saturation	(0-1)	0.7	1	0.85	0.4	1	0.7	0.667
High/low perm. ratio		1	20	10.5	1	20	10.5	1



# EOR: analytic screening. Worldwide database IRIS



The screenshot shows the IRIS software interface. The top navigation bar includes a 'Sword' logo, a 'Welcome, Ext user!' message, and buttons for 'Load', 'Save', 'Reports', 'Profile', 'Help', and 'Logout'. On the left, a sidebar menu lists 'Application screening' (0.01), 'Recovery factor estimation' (selected), 'Settings', 'Database', 'Cluster analysis', 'Field case analysis', 'Performance prediction', and 'Thermal recovery'. The main content area is titled 'Recovery Factor Estimation → Field Case Analysis'. It features a 'Parameters' table with input fields for Porosity, Permeability, Depth, Oil gravity, Oil viscosity, and Oil temperature. Below this is a button 'Analyze new field case'. A 'Distribution' table is also displayed, showing various methods and their associated recovery factors and confidence indices.

**Parameters**

	Porosity (0-1)	Permeability (md)	Depth (m)	Oil gravity (kg/m <sup>3</sup> )	Oil viscosity (cp)	Oil temperature (Celsius)
1	0.20	300.00	1200.000	800	5.00	

**Analyze new field case**

**Distribution**

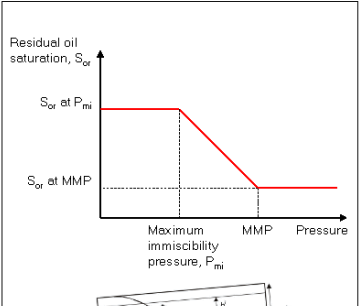
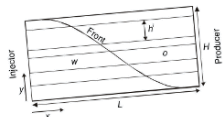
	Method	Number of cases	Mean recovery factor (0-1)	Standard deviation (0-1)	Confidence index (0-1)
1	Hydrocarbon Miscible	39	0.75	0.27	0.57
2	Polymer	3	0.16	0.08	0.18
3	Polymer, Surfactant	2	0.47	0.61	0.11
4	CO <sub>2</sub> Miscible	116	0.42	0.18	0.08
5	Combustion	16	0.49	0.14	0.04
6	CO <sub>2</sub> Immiscible	6	0.26	0.02	0.01
7	Surfactant	1	0.44	0.00	0.00

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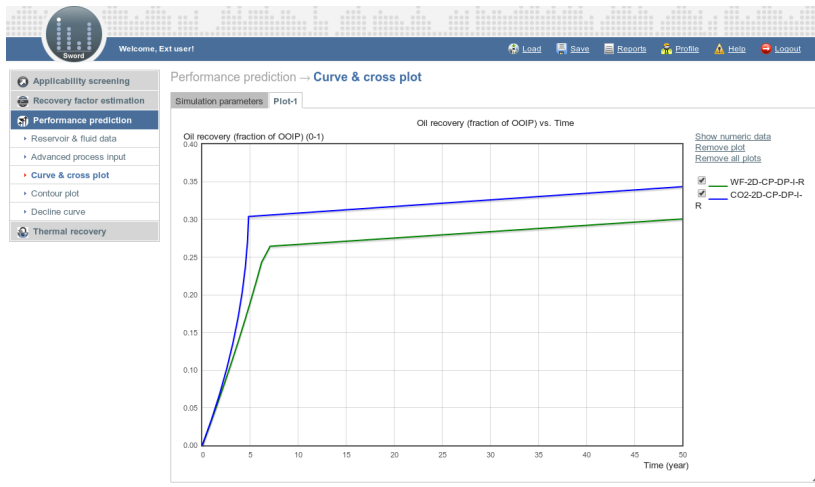
# EOR: analytic screening. Analytical simulation IRIS

Performance prediction → **Advanced process input**

Polymer	Surfactant	Nitrogen (miscible)	CO2 (miscible)	Hydrocarbon (miscible)	Cyclic waterflooding	WAG
<p>Minimum miscibility pressure (MMP)</p> <p><input checked="" type="checkbox"/> Use custom MMP ?</p> <p>Molecular weight C5+ <input type="text" value="213.5000"/> kg/kmol ?</p> <p>Oil volatile mole fraction <input type="text" value="0.33"/> (0-1) ?</p> <p>Oil intermediate mole fraction <input type="text" value="0.28"/> (0-1) ?</p> <p>Temperature <input type="text" value="60.00"/> Celsius ?</p> <p>MMP 163 bar</p> <p>Custom MMP <input type="text" value="220.0"/> bar ?</p>						
<p>Residual oil saturation at MMP <input type="text" value="0.03"/> (0-1) ?</p> <p>Maximum immiscibility pressure <input type="text" value="150.0"/> bar ?</p>						

# EOR: analytic screening. Analytical simulation IRIS



# Evaluation of CO<sub>2</sub> injection



As of the reservoir simulation:

- > Blackoil model may be used for quick evaluation of immiscible process.
- > Modern compositional simulations often allow lots of functionality. It is important:
  - Understand the physics of the process.
  - Concentrate on the governing forces and choose the tool which can handle them correctly
  - Use simpler correlations that fit to the data and knowledge you have rather than some 20-parametric model from which you can determine only 1 parameter.

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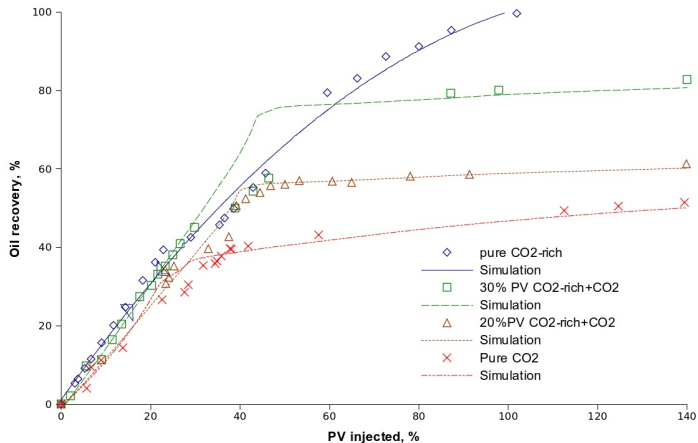


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# Three HC-phase flow

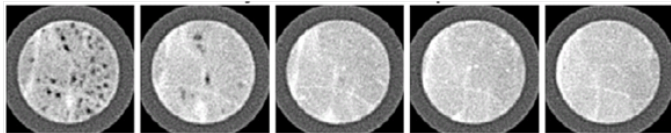
*Simulating lab scale results: building block for a pilot model*



# Interaction with reservoir rock

*Simulating lab scale results: building block for a pilot model* CT-scan

core measurements in DTU showed that carbonated water creates up to 1cm long wormholes:



Yet the injectivity into the core as a function of time *decreased*

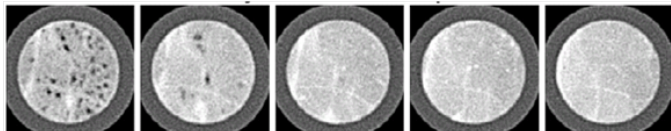


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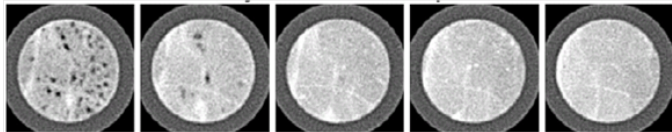


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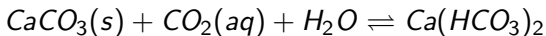
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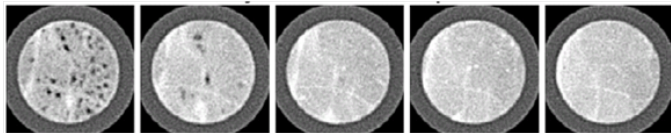


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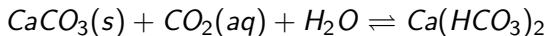
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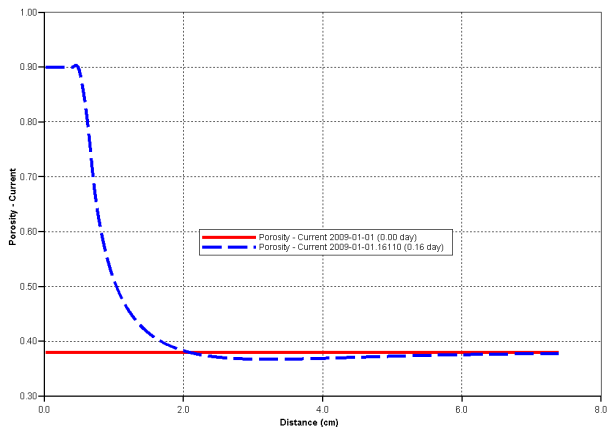
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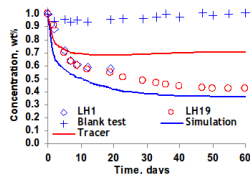
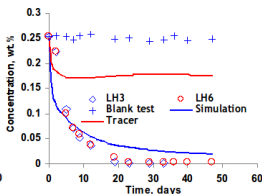
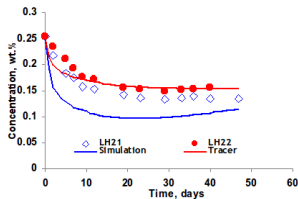
Those effects were successfully modeled with STARS:





# Mobility control: Foam

*Simulating lab scale results: building block for a pilot model* We can simulate a large set of experiments at different conditions using the same set of simulation parameters:


 $C_{surf} = 0.25 \text{ wt. \%}$ ,  $D_{plug} = 2.5 \text{ cm}$ 
 $C_{surf} = 0.25 \text{ wt. \%}$ ,  $D_{plug} = 3.8 \text{ cm}$ 
 $C_{surf} = 1.0 \text{ wt. \%}$ ,  $D_{plug} = 3.8 \text{ cm}$ 
 $S_w = 100\%$ ,  $T = 55^\circ \text{C}$ 

Questions regarding scaling those results up to reservoir level are being looked upon

# Reservoir simulation: data



Complex phase behaviour requires elaborate laboratory study:

- > Interaction between CO<sub>2</sub> and oil: miscibility development, changes in phase properties (swelling), precipitation
- > If mobility control agents are to be used lab studies are needed as well
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- > Temperature gradient in the reservoir, reservoir cooling due to cold CO<sub>2</sub> injection
- > Geochemical reactions
- > Stress (pressure) dependent reservoir properties
- > Compositional effects, dispersive mechanisms

# Reservoir simulation: accounting for



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- > Improved mobility control during gas injection
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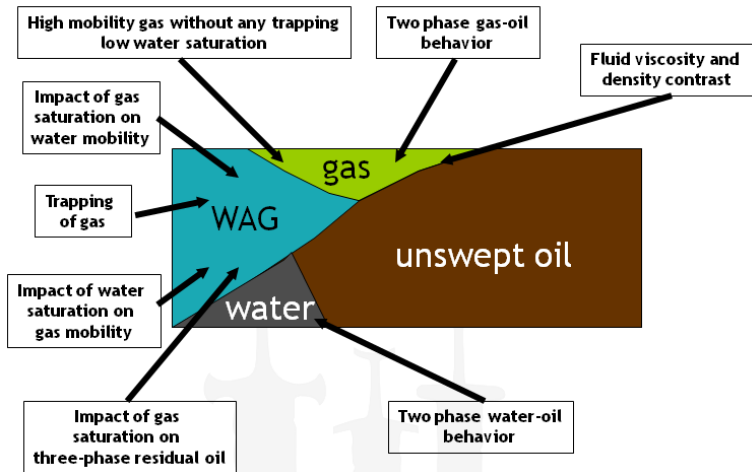
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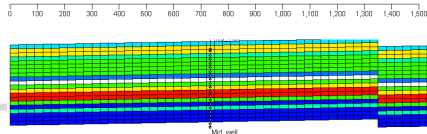


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## EOR: WAG



# EOR Project



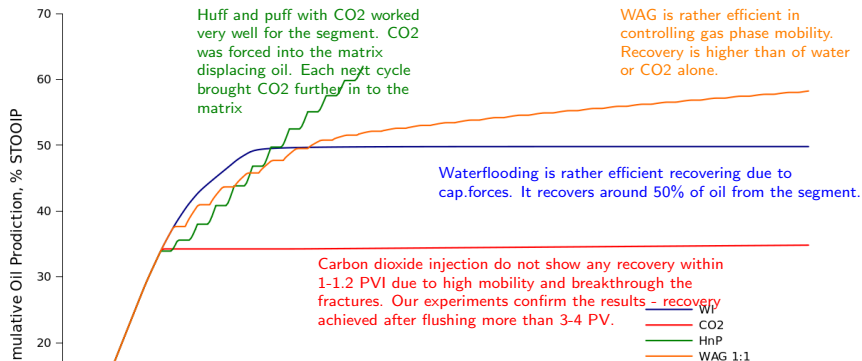
A compositional, dual porosity reservoir model accounting for various (viscous, gravity, capillary, diffusion forces) transfer mechanisms, solubility in water is constructed.

We account for changing porosity and permeability as a function of pressure.

Geochemical reactions are incorporated.

Importance of different effects is studied, different injection scenarios evaluated.

# EOR Project



# EGR: Pressure support

---



CO<sub>2</sub> can be injected (re-injected) into gas reservoir for pressure support

Gravity stable injection downflank to avoid breakthrough

Contamination of the produced gas with the CO<sub>2</sub> is the main risk

In case of antropogenic CO<sub>2</sub> stream impurities may provide additional challenge... or benefits... or both

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# EGR: Hydrates

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- > Thermal stimulation (energy)
- > Depressurisation (loss of productivity)
- > Inhibitor injection (environment, costs)
- > Gas exchange:
  - ca. 60% methane could be released
  - Heat of forming  $\text{CO}_2$  hydrates > energy consumption of  $\text{CH}_4$  dissociation

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- > CO<sub>2</sub> can significantly increase recovery of methane from coal beds
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# Concluding remarks

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Both EOR and EGR may be technically and economically feasible

It is important to study and verify **especially** compositional variations

There are other questions remaining:

- > CO<sub>2</sub> source (volume required is varying with time) and costs
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